# Electrodeposition and characterization of Ni-TiO<sub>2</sub> composite coatings

Zaverach Ie.M., Yermak N.V.

Khmelnytskyi National University, Khmelnytskyi, Instytutska Str. 11, 29016 evgzaverach@ukr.net

Electrodeposition of nickel-titania (Ni-TiO<sub>2</sub>) composite coatings was carried out from an additive-free Watts solution containing 10 and 20 g/l dispersed TiO<sub>2</sub> particles (size  $2 - 3 \mu m$ ). The influences of current density, bath temperature, TiO<sub>2</sub> concentration in the bath were studied. The corrosion performance, wear behavior and electrocatalytic properties of Ni-TiO<sub>2</sub> composite coatings were investigated. The results indicated that Ni-TiO<sub>2</sub> composite coatings with TiO<sub>2</sub> content 8 –10 wt.% exhibited higher corrosion and wear resistance than Ni coatings. Ni-TiO<sub>2</sub> composites showed electrocatalytic activity for the methanol oxidation.

## 1. Introduction

Electrodeposition is one of the most important techniques for producing metal matrix composites, owing to many merits, such as low cost, low operating temperature, ease of fabrication and high quality deposits. The metal matrix composites are materials in which the properties of a metallic host material are modified with addition of the second dispersed phase (micro, submicron- or nanosized particles) by electrodeposition process. Nickel is commonly used as continuous metallic matrix phase of composite coatings because of the high rates of deposition; nickel has excellent mechanical properties and high corrosion resistance; the appearance and other properties of electrodeposited nickel can be varied over wide ranges by controlling the composition and operating parameters of the plating solution [1, 2]. The dispersed phase can be hard oxides (Al<sub>2</sub>O<sub>3</sub>, TiO<sub>2</sub>, SiO<sub>2</sub>) [3 – 5], carbides (SiC, WC) [6 – 8], nitrides (BN, AlN) [9, 10] or polymers (PE, PTFE) [11, 12]. Many types of composite coatings have been developed to enhance corrosion

resistance, microhardness, wear resistance, self-lubrication, etc. The percentage and distribution of dispersed particles in metal matrix of composite coatings determine their mechanical and physicochemical properties. Moreover, the rate of particles' incorporation depends on the nature of particles (size, shape, charge) and the deposition conditions (current density, temperature, pH) [1 - 4, 8 - 10, 11].

Nickel based electrodes can be used as catalyst due to its surface oxidation properties. Their electrocatalytic activity depends mainly on the catalytic role of Ni(OH)<sub>2</sub>/NiOOH redox couple. Nickel displays potential catalytic properties in a wide number of processes: hydrogen evolution reaction, oxygen evolution reaction, hydrogenation reactions, electrosynthesis of amines, electrooxidation of small organic molecules (alcohols, aldehydes, amino acids, sugars) [13 – 19]. Electrooxidation of small organic molecules gives a promising way for direct converting the chemical energy of a fuel and an oxidant into electric energy in fuel cells. Nickel composite coatings show a higher catalytic activity than pure Ni coatings towards the electrochemical oxidation of methanol due to smaller grain size and larger actual surface area [17 - 19].

Thus, nickel based composite coatings are becoming important for different engineering applications: corrosion protection, hardening of machinery, increasing wear resistance, tool production, electrocatalysis. The aim of this work is to investigate the influence of deposition conditions on the incorporation of micro-sized  $TiO_2$  particles in nickel matrix and to study corrosion and electrocatalytic properties, wear behavior of Ni-TiO<sub>2</sub> composites.

### 2. Experimental details

Nickel coatings and composite Ni-TiO<sub>2</sub> coatings were electrodeposited from an additive-free Watts solution with a composition (in g/l): NiSO<sub>4</sub>·7H<sub>2</sub>O 240 – 260; NiCl<sub>2</sub>·6H<sub>2</sub>O 40 – 60; H<sub>3</sub>BO<sub>3</sub> 30 – 40. The deposition conditions were cathode current density, i, 0.8 - 2.5 A/dm<sup>2</sup>, pH 4 – 5, bath temperature, t, 20 and 50 °C, concentration of TiO<sub>2</sub> powder (size 2 – 3 µm) in bath, C<sub>TiO2</sub>, 10 and 20 g/l; metallurgical nickel anodes. The electrolyte was stirred by a magnetic stirrer in the electrodeposition process in order to maintain the uniform particles concentration and prevent

sedimentation in solution. Plain carbon steel and tool steel samples were the cathodes. The thickness of coatings was 20 and 30  $\mu$ m.

Before the electrodeposition, the samples were degreased in alkaline solution, dipped in acid solution (10% HCl with 5 g/l urotropine) and finally washed with distilled water. After electrodeposition, the samples were rinsed by distilled water and dried with air at room temperature.  $TiO_2$  content (wt.%) in the deposits was determined by gravimetric measurements.

Electrochemical studies were carried out in a conventional three-electrode cell powered by potentiostat/ galvanostat PI-50-1.1. An Ag/AgCl-Saturated KCl, a Pt wire and a sample (S = 1 cm<sup>2</sup>) with electrodeposited coating were used, respectively, as the reference, counter and working electrodes. The corrosion performance of electrodeposited coatings was investigated by potentiodynamic (potential sweep rate, v, was 5 mV/s) and potentiostatic polarization. A model corrosion medium of 5% NaCl solution with pH ~ 6 at temperature 15 – 20 °C was used. The investigations of methanol oxidation reaction were performed by using cyclic voltammetry at v = 10 mV/s. Measurements were carried out at temperature 15 – 20 °C in 1M NaOH solution in the absence and the presence of 1M of methanol. Prior to performing the polarization measurements, all investigated samples were maintained for a definite period in the solution. Potentials are presented in a standard hydrogen scale. The corrosion potential ( $E_{cor}$ ) and corrosion current density ( $i_{cor}$ ) were obtained using the Tafel exploration method. Corrosion rate K (mm/year) was calculated from the following equation

$$K = 8,76 \cdot \frac{i_{cor} \cdot q_{Ni}}{\rho_{Ni}} \tag{1}$$

where  $i_{cor}$  is corrosion current density in A/m<sup>2</sup>,  $q_{Ni}$  is electrochemical equivalent in g/(A·h),  $\rho_{Ni}$  is the density in g/cm<sup>3</sup>.

For measuring the wear resistance, dry sliding wear tests were carried out by using a pin on disk type machine on cylindrical samples against a steel wheel. The changes of linear size of sample due to wear of the pin was measured by differential capacitance sensor. The sliding parameters were rotation speed of the disc 40 m/min, the applied load 60 N, the sliding distance 1000 m.

#### 3. Results and discussion

The effect of deposition conditions on Ni-TiO<sub>2</sub> coatings composition is shown in Table 1. According to the obtained data, the content of TiO<sub>2</sub> particles in the coatings grows considerably due to the increase of concentration of dispersed phase in electrolyte. Apparent influence of current density and bath temperature on incorporation of TiO<sub>2</sub> particles in nickel matrix was observed.

i, A/dm <sup>2</sup>	$C_{TiO2}$ , g/l	t, °C	Ni (wt.%)	$TiO_2$ (wt.%)
0,8	10	20	95 – 97	3-5
1,0	10	20	98 - 99	1 – 2
1,0	10	50	86 - 88	13 – 15
1,5	10	50	90 - 92	8 - 10
1,5	20	50	75 – 78	22 – 25
2,5	10	50	97 – 99	1 – 3
2,5	20	50	82 - 85	15 – 18

Table 1. Effect of deposition conditions on

$\mathbf{N}$	. •		• . •
	00011000	001001	nontion
		(()))))	
	coutings	VUIII	DOSILIOII
-	- 0		

These results may be explained by the adsorption mechanism of dispersed particles and metal codeposition [1, 11, 18]. These phenomena play a considerable role in particle codeposition with nickel, due to the high adsorption affinity of nickel for the solid particles. According to this mechanism, the rate of codeposition is determined by initiation of real contact between the metal ions adsorbed on dispersed particles and the cathode surface. Once the particles are absorbed on the cathode surface, they will be imbedded into metal of coatings. With increased amount of TiO<sub>2</sub> dispersed particles in the electrolyte, nickel will be deposited with a higher amount of dispersed particles and a large area of the cathode surface will be covered by them.

It is known, that the increase of current density increases the Coulombic force between  $Ni^{2+}$  absorbed on dispersed particles and the cathode. Thus, the rate of

movement of  $TiO_2$  particles from bulk solution to the cathode surface increases, agglomeration of dispersed particles in the solution near the cathode may happen. Big agglomerates were not encapsulated and incorporated in metal matrix. Effect of bath temperature is conditioned on better efficiency of nickel deposition.

Fig. 1a presents potentiodynamic anodic polarization curves of galvanic nickel and Ni-TiO<sub>2</sub> composite coatings deposited at i = 1,5 A/dm<sup>2</sup> and C<sub>TiO2</sub> 10 and 20 g/l. Potentiostatic polarization curves (Fig. 1b) were obtained to evaluate corrosion data. The E<sub>cor</sub>, i<sub>cor</sub> and K values were calculated using the Tafel extrapolation method and equation (1) and they are given in Table 2.

Coating	E <sub>cor</sub> , V	$i_{cor}$ , A/m <sup>2</sup>	K, mm/year
Ni	-0,175	0,141	0,15
Ni-TiO <sub>2</sub> ,	-0,085	0,076	0,08
$TiO_2$ content 8 – 10 wt.%			

**Table 2.** Corrosion data of Ni and Ni-TiO<sub>2</sub> coatings

It was found, that incorporation in nickel matrix of dispersed TiO<sub>2</sub> particles results in shift of corrosion potentials to more positive values, decreases currents of anodic dissolution and corrosion currents in comparison with the pure Ni coatings. One should note here that anodic currents were higher for Ni-TiO<sub>2</sub> coatings deposited at  $C_{TiO2}$  10 g/l (TiO<sub>2</sub> content 22 – 25 wt.%) at E > 0,2 V than for nickel coatings (curve 1, 3 Fig. 1a). It can be attributed to the high content of TiO<sub>2</sub> in deposits which enhances their surface roughness.

The improvement of corrosion behavior of Ni-TiO<sub>2</sub> composite coatings can be connected with screening effect of metal matrix by dispersed particles with low electric conductivity and decrease in pitting at incorporation of dispersed particles. Besides, incorporation of TiO<sub>2</sub> into nickel coatings may reduce the size of Ni grains, due to the distribution of TiO<sub>2</sub> particles on the boundaries of Ni grains in the electrodeposition [18].



**Fig. 1.** Potentiodynamic anodic polarization curves, v = 5 mV/s; (b) potentiostatic polarization curves in 5% NaCl. Ni coatings (1) and Ni-TiO<sub>2</sub> coatings (2, 3) deposited at  $i = 1,5 \text{ A/dm}^2$  and  $C_{\text{TiO2}}$ : 10 g/l (2) and 20 g/l (3)

The relations between sliding distance and wear of samples with Ni and Ni-TiO<sub>2</sub> coatings is drawn in Fig.2. The results indicate that the wear of the coated surface increases with sliding distance. On the other hand, the wear of some Ni-TiO<sub>2</sub> composite coatings is lower than Ni coatings (curve 3 Fig. 2a; curve 3 Fig. 2b). At sliding distance 1000 m Ni coatings show the wear around 0,150 mm, but the Ni-TiO<sub>2</sub> composite coating deposited at t = 20 °C and current density 1 A/dm<sup>2</sup> (TiO<sub>2</sub> content 1 – 2 wt.%) show the wear 0,058 – 0,060 mm and Ni-TiO<sub>2</sub> composite coating deposited at t = 1,5 A/dm<sup>2</sup> (TiO<sub>2</sub> content 8 – 10 wt.%) show the wear 0,065 – 0,070 mm. By comparison, wear of uncoated samples was 0,450 – 0,495 mm.



Fig. 2. Relations between sliding distance and wear of samples with Ni coating (1) and with Ni-TiO<sub>2</sub> coating (2,3). (a) Ni-TiO<sub>2</sub> coating deposited at t = 20 °C and i: 0,8 A/dm<sup>2</sup> (2), 1 A/dm<sup>2</sup> (3); (b) Ni-TiO<sub>2</sub> composite coating deposited at t = 50 °C and i: 1  $A/dm^2$  (2), 1,5 A/dm<sup>2</sup> (3)

It was established, that wear behavior of Ni-TiO<sub>2</sub> composites depends on deposition conditions which determinate TiO<sub>2</sub> content into deposits and size of Ni grains [1, 2]. The improvement of wear behavior for some Ni-TiO<sub>2</sub> composites with TiO<sub>2</sub> content 1 - 10 wt.% may result from optimum number and distribution of dispersed particles in Ni matrix. TiO<sub>2</sub> particles with high hardness are barriers for shift of coating microlayers that lead to changing the friction conditions in sliding couple.

Fig. 3 shows cyclic voltammograms of Ni and Ni-TiO<sub>2</sub> coatings in 1M NaOH in the absence and presence of methanol. Two small peaks are observed in the voltammograms of Ni and Ni-TiO<sub>2</sub> coatings in 1M NaOH in anodic direction. One – at about 0,10 - 0,12 V due to formation of NiO and Ni(OH)<sub>2</sub> and the other – at about 0,65 - 0,7 V due to conversion of Ni(OH)<sub>2</sub> to NiOOH and enrichment of Ni<sup>3+</sup> species on the electrode surface.



Fig. 3. Cyclic voltammograms in the absence (1) and the presence of 1M of methanol (2). (a) Ni coating; (b) Ni-TiO<sub>2</sub> coating; deposition conditions were i = 1,5 A/dm<sup>2</sup>, t = 50 °C,  $C_{TiO2}$  = 10 g/l, v = 10 mV/s

The electro-oxidation of methanol on pure Ni and Ni-TiO<sub>2</sub> coatings starts at about 0,65 V when the electrode surface is covered with formed NiOOH species, then the current density reaches its maximum values at around 0,87 - 0,9 V in anodic direction. The response of methanol electro-oxidation at Ni-TiO<sub>2</sub> composite coatings is larger than the response obtained for pure electrodeposited nickel. Thus the oxidation current density of CH<sub>3</sub>OH at 0,87 V was 18 mA/cm<sup>2</sup> on Ni coating and 35 mA/cm<sup>2</sup> on Ni-TiO<sub>2</sub> coatings (curve 2 Fig. 3a and 3b).

It is seen from Fig.3 that another reoxidation peak appeared in the reverse scan at about 0,8 V. This peak was, probably, due to the reoxidation of CH<sub>3</sub>OH or the intermediate products generated during methanol oxidation. Formate and CO<sub>2</sub> were identified as the main reaction products in alkaline solutions [18], but it is possible that formation of absorbed CO may occur. Absorbed CO causes deactivation and blocking of the active sites of electrode surface during oxidation process. In the reversible half cycle absorbed intermediates and products are removed and the oxidation of CH<sub>3</sub>OH continues at the initial stage of the cathodic half cycle. The rate of methanol oxidation in the reverse scan drops as the unfavorable potentials (E < 0.5 V) are reached.

It was suggested that methanol is oxidized on Ni and Ni-TiO<sub>2</sub> coatings through the reaction with NiOOH to form Ni(OH)<sub>2</sub>, that is NiOOH acts as electron transfer mediator for the oxidation process [16 - 18]

$$NiOOH + methanol \leftrightarrow Ni(OH)_2 + products$$
 (2)

The enhancement of the catalytic activity of Ni-TiO<sub>2</sub> composite coatings was probably attributed to the presence of the mixed oxides (the nickel oxides and titanium oxides) which can be good electron transfer mediators for the oxidation process of organic molecules [18, 19]. In addition, the presence of TiO<sub>2</sub> dispersed particles can reduce the grain size of Ni and increase the actual surface area of electrodes that lead to formation of the great amount of active sites.

#### 4. Conclusions

Composite coatings consisting of nickel matrix and TiO<sub>2</sub> particles were obtained by means of electrodeposition. The content of TiO<sub>2</sub> particles in the coatings depends on current density, bath temperature, TiO<sub>2</sub> concentration in the bath. From results of electrochemical studies and wear tests, a conclusion can be drawn that Ni-TiO<sub>2</sub> composite coatings with TiO<sub>2</sub> content of 8 - 10 wt.% have improved corrosion and wear behavior. These composite coatings were deposited at current density of 1,5 A/dm<sup>2</sup>, bath temperature of 50 °C and concentration of dispersed particles of 10 g/l.

Ni-TiO<sub>2</sub> composite coatings showed a higher catalytic activity than pure Ni coatings towards the electro-oxidation of methanol. The process of methanol oxidation occurs at E = 0,65 - 0,9 V in anodic direction and continues in the initial stage of the cathodic half cycle of voltammograms.

## References

[1] L.I. Antropov, Yu.N. Lebedinskii, Kompozitsionnyie pokrytiia i matierialy, Kyiv: Technika, 1986, 200 c.

[2] A.M.A. Mohamed, T.D. Golden (Eds.), Electrodeposition of Composite Materials, Publisher: InTech, 2016, 282 p. [Online]. Available: https://www.intechopen.com/books/electrodeposition-of-composite-materials. [Accessed: 27-Feb-2018].

[3] R.K. Saha, T.I. Khan, Surf. Coat. Technol. 205 (2010) 890 – 895.

[4] P. Baghery, M. Farzam, A.B.Mousavi, M. Hosseini, Surf. Coat. Technol. 204 (2010) 3804 – 3810.

[5] W.-Y. Tu, B.-S. Xu, Sh.-Y. Dong, H.-D. Wang, Mat. Lett. 60 (2006) 1247 – 1250.

[6] E. Garcia-Lecina, I. Garcia-Urrutia, I.A. Diez, M. Salvo, F. Smeacetto, G. Gautier, R. Seddon, R. Martin, Electrochim. Acta 54 (2009) 2556 – 2562.

[7] F. Bratu, L. Benea, J.-P. Celis, Surf. Coat. Technol. 201 (2007) 6940 – 6946.

[8] M. Stroumbouli, P.Gyftou, E.A. Pavlatou, N. Spyrellis, Surf. Coat. Technol. 195 (2005) 325 – 332.

[9] E. Pompei, L. Magagnin, N. Lecis, P.L. Cavalotti, Electrochim. Acta 54 (2009) 2571 – 2574.

[10] A.A. Aal, M. Bahgat, M. Radwan, Surf. Coat. Technol. 201 (2006) 2910 – 2918.

[11] Z.A. Hamid, I.M. Ghayad, Mat. Lett. 53 (2002) 238 – 243.

[12] Q. Zhao, Y. Liu, Surf. Coat. Technol. 200 (2005) 2510 – 2514.

[13] R. Solmaz, A. Döner, G. Kardaş, Electrochem. Commun. 10 (2008) 1909 – 1911.

[14] J. Kubisztal, A. Budniok, Int. J. Hydrogen Energy 33 (2008) 4488 – 4494.

[15] I. Danaee, M. Jafarian, F. Forouzandeh, F. Gobal, M.G. Mahjani, Electrochim. Acta 53 (2008) 6602 – 6609.

[16] I. Danaee, M. Jafarian, F. Forouzandeh, F. Gobal, M.G. Mahjani, Int. J. Hydrogen Energy 33 (2008) 4367 – 4376.

[17] A.A. Aal, H.B. Hassan, M.A.A. Rahim, J. Electroanal. Chem. 619–620 (2008) 17–25.

[18] A.A. Aal, H.B. Hassan, J. Alloys Compd. 477 (2009) 652 – 656.

[19] H.B. Hassan, Z.A. Hamid, R.M. El-Sherif, Chinese J. Cat. 37 (2016) 616 – 627.